

## جذب سطحی یون‌های فلزی مس، روی و سرب از نمونه‌های آبی با استفاده از نانوذرات مغناطیسی Fe<sub>3</sub>O<sub>4</sub> اصلاح شده با آلizarin قرمز اس

صدیقه کامران

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## Adsorption of Copper, Zinc and Lead Metal Ions from Aqueous Samples Using Fe<sub>3</sub>O<sub>4</sub> Magnetic Nanoparticles Modified with Alizarin Red S

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### چکیده

نانوذرات مغناطیسی Fe<sub>3</sub>O<sub>4</sub> اصلاح شده با آلizarin قرمز اس برای حذف چند یون فلزی از محلول آبی استفاده شد. اندازه و ریخت‌شناسی نانوذرات بوسیله تکنیک‌های TEM، XRD و FTIR تعیین گردید. مطالعات جذب سطحی یون‌های مورد نظر در سیستم ثابت انجام گرفت. جذب سطحی بر سطح نانوذرات (ARS-Fe<sub>3</sub>O<sub>4</sub>) تحت تأثیر چندین پارامتر تجزیه‌ای مانند: pH اولیه، غلظت یون‌های فلزی، مقدار جاذب، زمان تماس و درجه حرارت می‌باشد. نتایج آزمایشات نشان داد که نانوذرات (ARS-Fe<sub>3</sub>O<sub>4</sub>) بطور کمی یون‌های مورد نظر را حذف می‌نماید. ماکزیمم ظرفیت جذب سطحی نانوذرات بر طبق مدل لانگمیر ۵۰/۰، ۲۲/۷ و ۲۱/۷ میلی‌گرم هریک از یون‌های Zn<sup>2+</sup>، Cu<sup>2+</sup> و Pb<sup>2+</sup> بر گرم نانوذرات می‌باشد. محاسبات همدمان نشان داد که داده‌های تعادلی با مدل لانگمیر نسبت به سایر مدل‌ها تطابق بهتری دارد. داده‌های سینتیکی جذب سطحی یون‌های Zn<sup>2+</sup>، Cu<sup>2+</sup> و Pb<sup>2+</sup> بر روی جاذب تهیه شده با معادله سینتیکی شبه درجه دوم بهتر توصیف می‌شود. فرآیند جذب سطحی در مورد هر سه یون مورد مطالعه گرماگیر است و این یون‌های فلزی توسط ۲ میلی‌لیتر محلول اسید کلریدریک ۰/۱ مول بر لیتر از سطح جاذب واجذب می‌گردد.

### واژه‌های کلیدی

نانوذرات مغناطیسی؛ آلizarin قرمز اس؛ جذب سطحی؛ حذف یون‌های فلزی.

### Abstract

Fe<sub>3</sub>O<sub>4</sub> magnetic nanoparticles modified with alizarin red S (ARS-Fe<sub>3</sub>O<sub>4</sub>) were used for the removal of several metal ions from aqueous solution. The mean size and the surface morphology of the nanoparticles were characterized by TEM, XRD and FTIR techniques. Adsorption studies of mentioned metal ions were performed in batch system. The adsorption of metal ions onto ARS-Fe<sub>3</sub>O<sub>4</sub> nanoparticles was affected by the several analytical parameters such as an initial pH, metal ions concentration, adsorbent amount, contact time and temperature. Experimental results indicated that ARS-Fe<sub>3</sub>O<sub>4</sub> nanoparticles were quantitatively removed. The maximum adsorption capacities of ARS-Fe<sub>3</sub>O<sub>4</sub> for the Langmuir model were 50.0, 22.7 and 21.7 mg of metal ions per gram of nanoparticle for Zn<sup>2+</sup>, Cu<sup>2+</sup> and Pb<sup>2+</sup>, respectively. The isotherm evaluations revealed that the Langmuir model attained better fits to the equilibrium data than the other models. The kinetic data of adsorption of Zn<sup>2+</sup>, Cu<sup>2+</sup> and Pb<sup>2+</sup> ions on the synthesized adsorbents were best described by pseudo-second-order equation. The adsorption processes for three metal ions were endothermic. Metal ions were desorbed from nanoparticles by 2 mL HCl solution 0.1 mol L<sup>-1</sup>.

### Keywords

Magnetic Nanoparticle; Alizarin Red S; Adsorption; Removal of Metal Ions.

### 1. INTRODUCTION

The heavy metal ions are not only dangerous for aquatic organisms, but also cause toxic effects to land animals including humans through food chain transfers. Heavy metal ions can specially bind to proteins, nucleic acids and small metabolites, in

living organisms. The contaminated organic cells are altered or missed their biological functions with losing the homeostatic control of essential metals, resulting in fatal health problems. Therefore, it is necessary to eliminate such hazardous heavy metal ion in wastewater before

discharging it into the environment. Water contaminated by heavy metal ions had become much more serious with a rapid development of industries and competitive use of fresh water in many parts of the world [1-4]. Waste waters from many industries such as metallurgical, tannery, chemical manufacturing, mining, battery manufacturing industries, etc. contain one or more toxic heavy metal ions. It is necessary to remove these ions from the waste waters before releasing them into the environment. There has been increasing concern and more stringent regulation standards pertaining to the discharge of heavy metal ions into the aquatic environment [3-4]. Many technologies and methods for heavy metal ions removal from waste waters have been developed, such as ion-exchange, evaporation and concentration, chemical precipitation, reverse-osmosis, adsorption and electro dialysis.

Considering from economy and efficiency point of view, adsorption is regarded as one of the most promising and widely used methods. A number of materials, including activated carbon [5-6], fly ash [7-8], peat [9], sewage sludge ash [10], zeolites [11], biomaterials [12-13], recycled alum sludge [14], manganese oxides [15], peanut hulls [16], kaolinite [17] resins [18], alumina modified by surfactant [19], Octadecyl silica [20] and etc have been reported to be capable of adsorbing heavy metal ions from aqueous solutions. Nevertheless, these materials have some inherent disadvantages such as low adsorption capacities or high costs, which place urgent needs for the development of new adsorbent materials aimed at protecting our water and ensuring widespread access to clean and affordable potable water [21]. Therefore, research for new and more effective materials to be used as adsorbents is a continuous effort for many researchers. Nanomaterials have large specific surface areas and thus a large fraction of active sites are available for appropriate chemical interaction [22]. Surface modification of magnetic nanoparticles can be accomplished by physical/chemical adsorption of organic compounds by four major techniques: organic vapor condensation, polymer coating, surfactant adsorption and direct silanation [23].

This paper focuses on the preparation of magnetic nanoparticles of  $\text{Fe}_3\text{O}_4$  modified by alizarin red S (ARS- $\text{Fe}_3\text{O}_4$ ) and characterization by Thermal electron microscopy (TEM), Fourier transform infrared (FTIR) spectroscopy and X ray Diffraction (XRD). Removal of  $\text{Zn}^{2+}$ ,  $\text{Cu}^{2+}$  and  $\text{Pb}^{2+}$  onto  $\text{Fe}_3\text{O}_4$  modified alizarin red S was studied. The effects of different experimental conditions such as dosage of nanoparticle, concentrations of metal ions, pH of the aqueous sample and contact times, on removal of three

metal ions were evaluated. Adsorption isotherms, kinetic of adsorption and thermodynamic parameters were characterized as well. To the best of our knowledge, adsorption of these metal ions onto  $\text{Fe}_3\text{O}_4$  magnetic nanoparticles modified by ARS has not been reported.

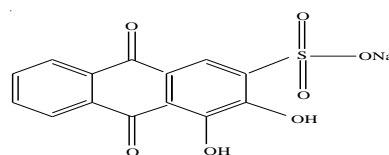
## 2. EXPERIMENTAL

### 2.1. Apparatus

An atomic absorption spectrometer of GBC SCIENTIFIC EQUIPMENT model was used for determination of  $\text{Zn}^{2+}$ ,  $\text{Cu}^{2+}$  and  $\text{Pb}^{2+}$ . The following conditions were used: absorption line; Cu: 327.4 nm, Zn: 213.9 nm, Pb: 405.8 nm; slit width: 0.5 nm; and lamp currents: 4 mA. The flow rates of air and acetylene were set as recommended by the manufacturer. A double beam UV-visible Shimadzu spectrophotometer Model 1601 equipped with a 1-cm quartz cell was used for recording the visible spectra and absorbance measurements. The infrared spectra were recorded by KBr pellets using FT-IR spectrometer model PerkinElmer Spectrum RXI. The XRD measurements were performed on the XRD Bruker D8 Advance. A transmission electron microscope (Philips CM 10 TEM) was used for recording the TEM images. A Metrohm 780 pH meter was used for monitoring the pH values. A water Ultrasonicator (Model CD-4800, China) was used to disperse the nanoparticles in solution and a super magnet Nd-Fe-B (1.47 T,  $10 \times 5 \times 2$  cm) was used. All measurements were performed at ambient temperature.

### 2.2. Chemicals and reagents

All chemicals and reagents were of analytical grades. Alizarin red S (scheme 1), sodium chloride,  $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$  (96 % w/w) and  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$  (99.9 % w/w) were purchased from Merck (Darmstadt, Germany). The stock solution of copper sulphate pentahydrate ( $\text{CuSO}_4 \cdot 5\text{H}_2\text{O}$ ), zinc nitrate hexahydrate ( $\text{Zn}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ ) and lead nitrate ( $\text{Pb}(\text{NO}_3)_2$ ) were prepared by dissolving an accurately weighed amount of the salts in deionized water. The experimental solutions were prepared by diluting the stock solution with distilled water when necessary. The pH adjustments were performed with HCl and NaOH solutions ( $0.01$ – $1.0 \text{ mol L}^{-1}$ ).



**Scheme 1.** Chemical Structure of alizarin red S.

### 2.3. Fabrication of ARS-modified magnetic nanoparticles

The nanoparticles of  $\text{Fe}_3\text{O}_4$  were synthesized by mixing ferrous sulfate and ferric chloride in NaOH solution with constant stirring as recommended [24]. To obtain maximum yield for magnetic nanoparticles during co-precipitation process, the ideal molar ratio of  $\text{Fe}^{2+}/\text{Fe}^{3+}$  was about 0.5. The precipitates were heated at  $80^\circ\text{C}$  for 30 minutes and were sonicated for 20 minutes, then washed three times with 50 mL distilled water solution.

Modification of  $\text{Fe}_3\text{O}_4$  nanoparticles was carried out using alizarin red S at room temperature. In order to modify the nanoparticles, 20 mL of ARS solution ( $30\text{ mg L}^{-1}$ , pH 3.0) was added to about 0.025 g of damped nanoparticles in a beaker and the solution was stirred for 30 min by a glassy rod, followed by stirring using a magnetic stirrer. The modified magnetite nanoparticles (ARS- $\text{Fe}_3\text{O}_4$ ) were collected by applying a magnetic field with an intensity of 1.4 T. The ARS- $\text{Fe}_3\text{O}_4$  nanoparticles were washed three times with 50 mL distilled water. Nanoparticles and distilled water mixture was dispersed by ultrasonicator for 10 minutes at room temperature. Finally, the ARS- $\text{Fe}_3\text{O}_4$  nanoparticles were magnetically separated.

### 2.4. Adsorption equilibrium of metal ions

Adsorption of metal ions onto ARS- $\text{Fe}_3\text{O}_4$  nanoparticles from aqueous solutions was investigated batch-wise. The magnetic nanoparticles (0.025g) were incubated with 5 mL of the aqueous solutions of metal ions for 2-25 minutes (equilibrium time) in a beaker agitated magnetically at 150 rpm. After mixing, magnet was removed and washed with distilled water. Then the adsorbed metal ions on the surface of ARS- $\text{Fe}_3\text{O}_4$  nanoparticles was magnetically separated and the mother solution was analyzed for the residual metal ions with FAAS.

### 2.5. Adsorption kinetics studies

To study the adsorption kinetics of a metal ions, the modified  $\text{Fe}_3\text{O}_4$  (0.025 g) was incubated with 5.0 mL of the solutions (at a specific pH), containing  $50\text{ mg L}^{-1}$  of each metal ions, and the suspension was immediately stirred (150 rpm) for different periods of time. Adsorption kinetic data were obtained by measuring the concentration of metal ions in the solution at different times after removing the magnetic nanoparticles.

### 2.6. Characterization of $\text{Fe}_3\text{O}_4$ and ARS- $\text{Fe}_3\text{O}_4$

The peaks positions and relative intensities observed in XRD patterns of ARS- $\text{Fe}_3\text{O}_4$  nanoparticles and standard  $\text{Fe}_3\text{O}_4$  are shown in

Fig. 1 for comparison. Five characteristics peaks for both  $\text{Fe}_3\text{O}_4$  and ARS- $\text{Fe}_3\text{O}_4$  corresponding to indices (220), (311), (400), (511) and (440) were observed. Analysis of XRD patterns of  $\text{Fe}_3\text{O}_4$  and ARS- $\text{Fe}_3\text{O}_4$  indicated very distinguishable peaks for magnetite crystal, which means that these particles have phase stability [25- 26].

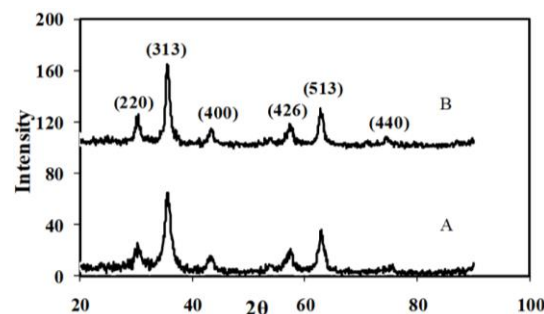


Fig. 1. XRD pattern of  $\text{Fe}_3\text{O}_4$ , A; and ARS- $\text{Fe}_3\text{O}_4$ , B.

The FTIR spectra of  $\text{Fe}_3\text{O}_4$ , ARS and ARS- $\text{Fe}_3\text{O}_4$  are shown in Fig. 2A-2C. In the case of  $\text{Fe}_3\text{O}_4$ , the broad absorption band at  $3200\text{--}3500\text{ cm}^{-1}$  indicates the presence of surface hydroxyl groups (O-H stretching). The bands at low wave numbers ( $700\text{ cm}^{-1}$ ) are related to vibrations of Fe-O bonds of magnetite nanoparticles.

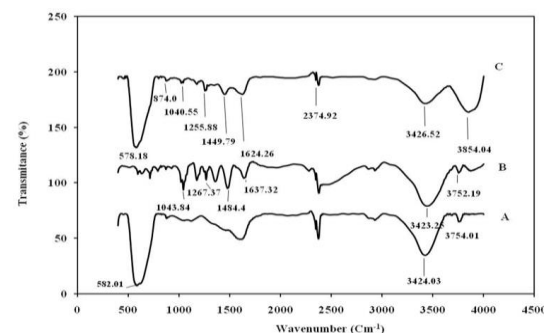


Fig. 2. FTIR spectra of  $\text{Fe}_3\text{O}_4$ , A; ARS, B; and ARS- $\text{Fe}_3\text{O}_4$ , C.

The presence of magnetite nanoparticles can be verified by appearance of two strong absorption bands around  $632$  and  $585\text{ cm}^{-1}$  [27- 28]. In the spectrum of ARS and ARS- $\text{Fe}_3\text{O}_4$  (Fig. 2A-2C), the broad peak at  $3200\text{--}3500$  is attributed to the stretching of bonded hydroxyl group. The band around  $2900\text{ cm}^{-1}$  shows C-H stretching of aromatic ring. C=O and C=C in ARS gives significantly stronger peaks in the ranges of  $1400\text{--}1650\text{ cm}^{-1}$ . In the FTIR spectrum of ARS- $\text{Fe}_3\text{O}_4$ , the significant absorption band at  $2925\text{ cm}^{-1}$  is due to the C-H stretching. The absorption bands indicate to the  $\text{SO}_3$  stretching and C-O stretching in ARS- $\text{Fe}_3\text{O}_4$  around  $1000\text{--}1300\text{ cm}^{-1}$  and the Fe-O bonds in magnetite nanoparticles shows at  $578\text{ cm}^{-1}$ . After modifying, the peak shift from  $578$  to  $582\text{ cm}^{-1}$  for Fe-O bond

vibration and similarly, a shifted in the peaks of S=O and O-H stretching towards lower or higher wavenumber, respectively, were observed indicating the developed interaction between  $\text{Fe}_3\text{O}_4$  and ARS. The results showed that the functional groups of ARS might be involved in developing attraction forces between  $\text{Fe}_3\text{O}_4$  nanoparticles and ARS through electrostatic interaction and hydrogen bonding. The modification with ARS at lower pH values was more significant probably due to the electrostatic attractions between negatively-charged ARS and positively-charged nanoparticles.

Fig. 3A is the representative TEM image of  $\text{Fe}_3\text{O}_4$  and ARS- $\text{Fe}_3\text{O}_4$  nanoparticles. The average diameter of  $\text{Fe}_3\text{O}_4$  nanoparticles was about ~10 nm. However, the TEM image (Fig. 3B) indicates that ARS- $\text{Fe}_3\text{O}_4$  (~15 nm) had a larger particle diameter than  $\text{Fe}_3\text{O}_4$ .

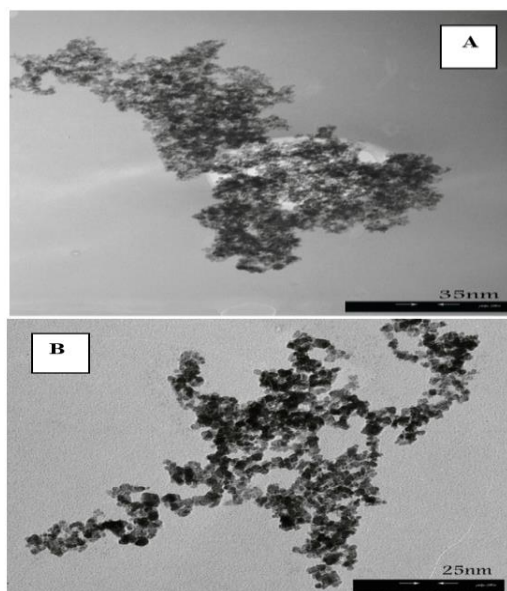


Fig. 3. The TEM image of  $\text{Fe}_3\text{O}_4$ , A and ARS- $\text{Fe}_3\text{O}_4$ , B.

### 3. RESULT AND DISCUSSION

Some heavy metals (e.g.,  $\text{Cu}^{2+}$  and  $\text{Zn}^{2+}$ ) are essential for plant and animal health. However, at environmental concentrations above those necessary to sustain life, toxicity may occur. Other heavy metals (e.g  $\text{Pb}^{2+}$ ) are not known to be essential to plants and animals and toxicity may occur when these metals become concentrated in the environment above the background levels [29]. So specifically,  $\text{Zn}^{2+}$ ,  $\text{Cu}^{2+}$  and  $\text{Pb}^{2+}$  were studied. The efficiency of the prepared ARS- $\text{Fe}_3\text{O}_4$  as adsorbents for removal of  $\text{Zn}^{2+}$ ,  $\text{Cu}^{2+}$  and  $\text{Pb}^{2+}$  from their individual aqueous solutions was investigated under different experimental conditions in order to find their optimum values as discussed below.

#### 3.1. Effect of contact time

Contact time is an important factor in evaluating the adsorption efficiency, which helps to determine the rate of maximum removal of solutes. The effect of contact time on the performance of ARS- $\text{Fe}_3\text{O}_4$  nanoparticles for adsorption of three metal ions was investigated. An ARS- $\text{Fe}_3\text{O}_4$  amount of 0.025 g and a solution pH of 4.5 were considered for following this investigation. The initial metal ions concentration for all tested solutions were  $50 \text{ mg L}^{-1}$ . Fig. 4 shows removal efficiencies for three metal ions as a function of stirring time in the range of 2-25 minutes.

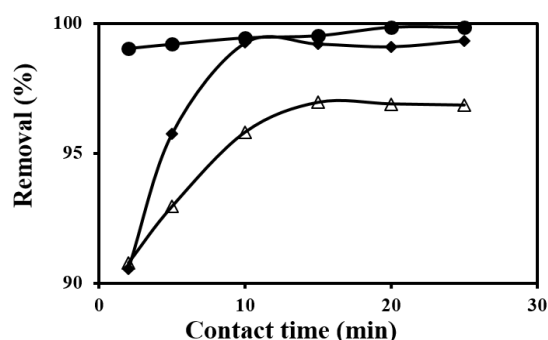


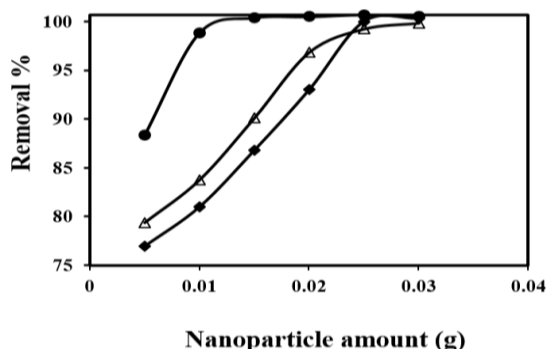
Fig. 4. Effect of stirring time on the adsorption of:  $\text{Pb}^{2+}$ , ( $\bullet$ );  $\text{Zn}^{2+}$ , ( $\blacklozenge$ ); and  $\text{Cu}^{2+}$ , ( $\Delta$ ). Experimental conditions: ARS- $\text{Fe}_3\text{O}_4$  amount of 0.025 g, initial metal ion concentration of  $50 \text{ mg L}^{-1}$  at pH value 4.5.

The results indicate that the adsorption processes for three metal ions started immediately upon addition of ARS- $\text{Fe}_3\text{O}_4$ . The removal efficiency for  $\text{Cu}^{2+}$  and  $\text{Zn}^{2+}$  rapidly increased from 90%, in the first minute of contact, to a value of 97% and 99%, respectively, after stirring time of 15 and 10 and where the equilibrium condition was attained. For  $\text{Pb}^{2+}$ , the percentage of removal, obtained in the first minute of stirring, was 99%; complete removal (99.8) was attained when the stirring was done for 5 minutes. Therefore, the optimum contact time between sample solution and ARS- $\text{Fe}_3\text{O}_4$  nanoparticles was considered to be 15, 10 and 5 minutes for  $\text{Zn}^{2+}$ ,  $\text{Cu}^{2+}$  and  $\text{Pb}^{2+}$ , respectively. The rapid adsorption, at the initial contact time, is due to the availability of functional groups of ARS on surfaces of nanoparticles which led to a complexation between metal ions and dye. The presence of ARS onto the surface of nanoparticles increases interactions between ARS- $\text{Fe}_3\text{O}_4$  and metal ions. This also shortens the contact time required for metal ions to be quantitatively removed by ARS- $\text{Fe}_3\text{O}_4$ .

#### 3.2. Effect of ARS- $\text{Fe}_3\text{O}_4$ amount

The effect of ARS- $\text{Fe}_3\text{O}_4$  amount on adsorption of  $\text{Zn}^{2+}$ ,  $\text{Cu}^{2+}$  and  $\text{Pb}^{2+}$ , from their individual

solutions, was investigated using a batch technique by adding a known quantity of the adsorbent, in the range of 5-30 mg, into individual beakers containing 5 mL of the metal ions solution. The resulted suspensions were immediately stirred with a magnetic stirrer for 15, 10 and 5 minutes for  $Zn^{2+}$ ,  $Cu^{2+}$  and  $Pb^{2+}$ , respectively. After the mixing time elapsed, the ARS- $Fe_3O_4$  nanoparticles were magnetically separated and the solutions were analyzed for the metal ions residue. For all measurements, the initial metal ions concentrations were fixed at  $50 \text{ mg L}^{-1}$  while the value of pH was 4.5. Results in Fig. 5 indicate that 82% of  $Cu^{2+}$ , 87% of  $Zn^{2+}$  and 98% of  $Pb^{2+}$  were removed from their individual aqueous solutions when an initial amount of 10 mg ARS- $Fe_3O_4$  was used. The percent removals of three metal ions increased with increasing ARS- $Fe_3O_4$  (up to the amount of 10 mg) and eventually reached to the values of 99.2%, 100.0% and 100 for  $Zn^{2+}$ ,  $Cu^{2+}$  and  $Pb^{2+}$ , respectively. This observation can be explained by the fact that more adsorption sites would be available for metal ions at higher amount of ARS- $Fe_3O_4$ .

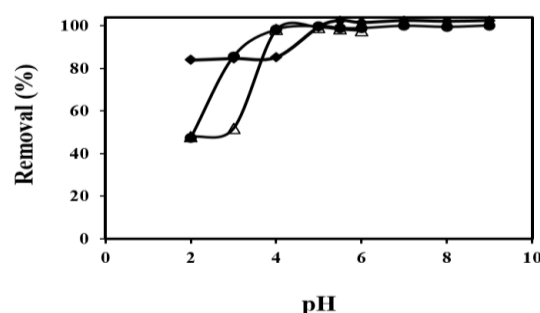


**Fig. 5.** Effect of nanoparticles amount on the adsorption of:  $Pb^{2+}$ , (●);  $Zn^{2+}$ , (◆); and  $Cu^{2+}$ , (Δ). Experimental conditions: initial metal ion concentration of  $50 \text{ mg L}^{-1}$  at pH value 4.5, stirring time of ( $Pb^{2+}$ , 5;  $Zn^{2+}$ , 10 and  $Cu^{2+}$ , 15 minutes).

### 3.3. Effect of initial pH

The pH plays an important role in metal adsorption which is related to both the metal species and the availability of binding site which depends on the functional group of the sorbent [30]. The metal species,  $M(II)$ ;  $Cu(II)$ ,  $Pb(II)$  and  $Zn(II)$  are present in forms of  $M^{2+}$ ,  $M(OH)^+$ ,  $M(OH)_2(\text{solid})$ , etc. in water [30]. The solubility of the  $M(OH)_2(\text{solid})$  is very high at pH  $\sim 5.0$ , so a large amount of the  $M^{2+}$  presents as main species. When pH is increasing the solubility of  $M(OH)_2(\text{solid})$  decrease resulting in the main species in the solution is  $M(OH)_2(\text{solid})$ . It can be tell that the  $M^{2+}$  must be much more reduce at higher pH, but the major process for removing the  $M^{2+}$  is the precipitation, not adsorption [31].

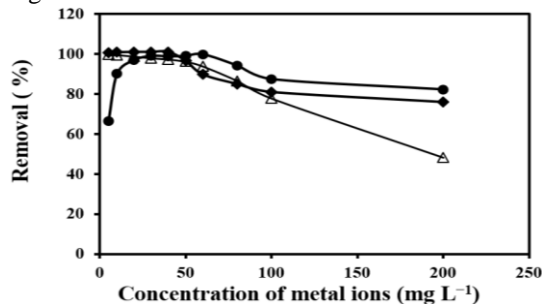
The influence pH of solution on the extent of adsorption of magnetic nanoparticle shown in Fig. 6. The removal of  $Zn^{2+}$ ,  $Cu^{2+}$  and  $Pb^{2+}$  from solution by adsorption is highly dependent on the pH of the solution. It was found that between 99.0% and 100% removal of the metal ions achieved in pH between 5.0 and 6.0. At pH values higher than 6.0 insoluble metal hydroxide starts, precipitating from the solutions making true adsorption studies impossible. At pH  $< 5.0$ , decrease in the removal efficiency could be due to the competition of hydronium ion toward complexation with alizarin red S. Therefore, the adsorption capacity was higher in pH range of 5.0-6.0 for all cases.



**Fig. 6.** Effect of pH of the sample solution on adsorption of  $Pb^{2+}$ , (●);  $Zn^{2+}$ , (◆); and  $Cu^{2+}$ , (Δ). Experimental conditions: ARS- $Fe_3O_4$  amount of 0.01 g, stirring time of ( $Pb^{2+}$ , 5;  $Zn^{2+}$ , 10; and  $Cu^{2+}$ , 15 minutes) initial metal ion concentration of  $50 \text{ mg L}^{-1}$ .

### 3.4. Effect of metal ions concentration.

The initial metal ions concentration is an important parameter that can affect its adsorption process. This will determine the concentration range of metal ions that could be quantitatively adsorbed, i.e. the concentration range for which the adsorption efficiency is high and independent of the initial concentration of metal ions. To obtain this, different concentrations of  $Zn^{2+}$ ,  $Cu^{2+}$  and  $Pb^{2+}$  were studied for their removal by ARS- $Fe_3O_4$  under optimum experimental conditions. The results, in terms of removal efficiency versus initial concentrations of metal ions, are shown in Fig. 7.

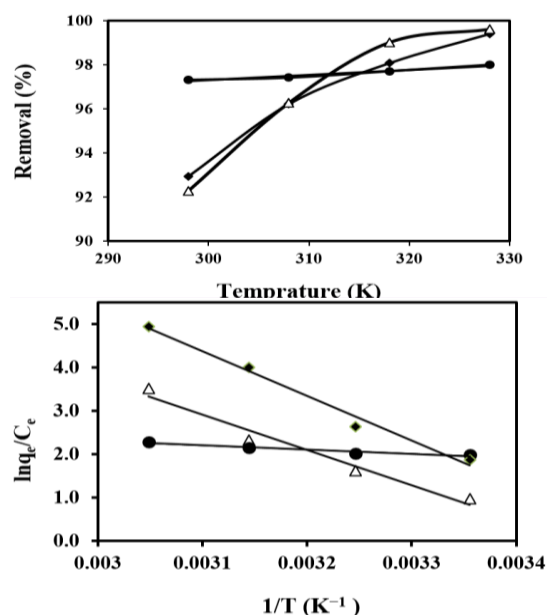


**Fig. 7.** Effect of initial metal ion concentration on adsorption of  $Pb^{2+}$ , (●);  $Zn^{2+}$ , (◆); and  $Cu^{2+}$ , (Δ). Experimental conditions: ARS- $Fe_3O_4$  amount of 0.01 g,

stirring time of ( $\text{Pb}^{2+}$ , 5;  $\text{Zn}^{2+}$ , 10; and  $\text{Cu}^{2+}$ , 15 minutes), pH value 5.0.

### 3.5. Effect of solution temperature

The effect of temperature on the adsorption of  $\text{Zn}^{2+}$ ,  $\text{Cu}^{2+}$  and  $\text{Pb}^{2+}$  ( $50 \text{ mg L}^{-1}$ ) from their individual solutions on  $0.025 \text{ g}$  of  $\text{ARS-Fe}_3\text{O}_4$  nanoparticles was studied at pH with a stirring time of 15, 10 and 5 minutes. A thermo shaker was used for adjusting of temperature and shaking. Fig. 8 shows the removal efficiencies for three metal ions as a function of temperature ranging between 298 and 328 K.



**Fig. 8.** (A) Effect of temperature on adsorption of:  $\text{Pb}^{2+}$ , (●);  $\text{Zn}^{2+}$ , (◆); and  $\text{Cu}^{2+}$ , (Δ). (B), the plots of  $\ln(q_e/C_e)$  against  $1/T$  for  $\text{Pb}^{2+}$ , (●);  $\text{Zn}^{2+}$ , (◆); and  $\text{Cu}^{2+}$ , (Δ). Experimental conditions: ARS- $\text{Fe}_3\text{O}_4$  amount of  $0.01 \text{ g}$ , initial metal ion concentration of  $50 \text{ mg L}^{-1}$  at optimized pH value 5.0 and stirring time of ( $\text{Pb}^{2+}$ , 5;  $\text{Zn}^{2+}$ , 10; and  $\text{Cu}^{2+}$ , 15 minutes).

The results indicate that solution temperature strongly affected the adsorption efficiency of three metal ions. For instance, the adsorption efficiencies of both  $\text{Cu}^{2+}$  and  $\text{Zn}^{2+}$  were about 93% at 298 K and eventually reached to values of 99.4% and 100.8% at 328 K, respectively, indicating to an endothermic nature of the adsorption processes. The changes in standard free energy as well as changes in enthalpy and entropy of adsorption were calculated using van't Hoff equation:

$$\Delta G^0 = -RT \ln K_c \quad (1)$$

$$\ln K_c = -\frac{\Delta H^0}{RT} + \frac{\Delta S^0}{R} \quad (2)$$

Where  $\Delta S^0$  and  $\Delta H^0$  are change in entropy and enthalpy of adsorption, respectively. The  $K_c$  is the ratio of adsorbate concentration on adsorbent

at equilibrium ( $q_e$ ) to the remaining adsorbate concentration in the solution at equilibrium ( $C_e$ ). The values of  $\Delta H^0$  and  $\Delta S^0$  were evaluated from the slope and intercept of van't Hoff plot (Table 1). The results indicate that the adsorption processes for three metal ions are endothermic. The negative value of  $\Delta G^0$  indicates that the adsorption processes for three metal ions are spontaneous. The direct dependency of the negative value of  $\Delta G^0$  to temperature indicates that the spontaneity of adsorption is proportional to temperature. The positive value of  $\Delta H$  indicates that adsorption processes for three metal ions onto ARS- $\text{Fe}_3\text{O}_4$  are endothermic. Thermodynamic studies revealed that greater adsorption can be obtained at higher temperatures. The values of entropy for adsorption of  $\text{Zn}^{2+}$ ,  $\text{Cu}^{2+}$  and  $\text{Pb}^{2+}$  were 233.3, 295.5 and  $40.2 \text{ J mol}^{-1}\text{K}^{-1}$ , respectively. The positive value of  $\Delta S^0$  suggests randomness increasing at the solid/solution interface during the adsorption of three metal ions [32-33].

**Table 1.** Thermodynamic parameters of metal ions-adsorption process onto ARS- $\text{Fe}_3\text{O}_4$  nanoparticle.

Metal ion	$\Delta S_0^T$ ( $\text{J mol}^{-1}\text{K}^{-1}$ )	$\Delta H_0^T$ ( $\text{kJ mol}^{-1}$ )	$\Delta G_0^T$ ( $\text{kJ mol}^{-1}$ )			
			298 K	308 K	318 K	328 K
$\text{Cu}^{2+}$	233.3	67.45	-2.68	-4.40	-6.73	-9.07
$\text{Zn}^{2+}$	295.48	83.60	-4.45	-7.4	-10.36	-13.32
$\text{Pb}^{2+}$	40.18	7.09	-4.9	-5.3	-5.7	-6.09

### 3.6. Adsorption isotherm modeling

Several isotherm models for evaluating the equilibrium adsorption, has discussed in literatures [34]. For evaluating the equilibrium adsorption, Langmuir and Freundlich isotherm models were used. The linearized form of the Langmuir isotherm, assuming monolayer adsorption on a homogeneous adsorbent surface, is expressed as:

$$\frac{C_e}{q_e} = \frac{1}{bq_{max}} + \frac{C_e}{q_{max}} \quad (3)$$

where  $q_{max}$  ( $\text{mg g}^{-1}$ ) is the surface concentration at monolayer coverage and illustrates the maximum value of  $q_e$  that can be attained as  $C_e$  is increased. The  $b$  parameter is a coefficient related to the

energy of adsorption and increases with increasing strength of the adsorption bond. Values of  $q_{\max}$  and  $b$  are determined from the linear regression plot of  $(C_e/q_e)$  versus  $C_e$ .

The Freundlich equation is expressed in its linear form as follows:

$$\log q_e = \log K_F + \frac{1}{n} \log C_e \quad (4)$$

where  $K_F$  and  $n$  are the constants from the Freundlich equation representing the capacity of the adsorbent for the adsorbate and the reaction order, respectively. The reciprocal reaction order,  $1/n$ , is a function of the strength of adsorption.

The equilibrium adsorption data for  $Zn^{2+}$ ,  $Cu^{2+}$  and  $Pb^{2+}$  were analyzed using Langmuir and Freundlich, models. Models fitted to equilibrium adsorption results of three metal ions were assessed based on the values of the correlation coefficients ( $R^2$ ) of their linear regression plots. The experimental data fitted with two models indicated that the adsorptions of  $Zn^{2+}$ ,  $Cu^{2+}$  and  $Pb^{2+}$  on ARS- $Fe_3O_4$  nanoparticles are better described by the Langmuir model. The resulting plots for Langmuir model are shown in Table 2 summarize the model constants and the correlation coefficient.

**Table 2.** Adsorption isotherm parameters for adsorption of  $Cu^{2+}$ ,  $Zn^{2+}$  and  $Pb^{2+}$  onto ARS- $Fe_3O_4$  nanoparticle.

Metal ion	Langmuir model			Freundlich model		
	$q_{\max}$ (mg g <sup>-1</sup> )	$b$	$R^2$	$K_F$ (mg g <sup>-1</sup> )	$n$ (g L <sup>-1</sup> )	$R^2$
Cu <sup>2+</sup>	22.7	0.33	0.986	57.4	1.8	0.935
Zn <sup>2+</sup>	50.0	1.33	0.989	2.04	1.42	0.840
Pb <sup>2+</sup>	21.7	1.0	0.989	11.0	1.66	0.913

Three metal ions were adsorbed on ARS- $Fe_3O_4$  nanoparticles due to its complexation with Alizarin red S. The maximum adsorption capacity of ARS- $Fe_3O_4$  nanoparticle for  $Zn^{2+}$ ,  $Cu^{2+}$  and  $Pb^{2+}$  is 50.0, 22.7 and 21.7 mg of metal ions per gram of nanoparticle.

Table 3 presents a comparison between the adsorption capacity (obtained based on the Langmuir model) of the developed adsorbent and

another adsorbent reported in literature for adsorption of  $Zn^{2+}$ ,  $Cu^{2+}$  and  $Pb^{2+}$  [29, 35,36].

**Table 3.** Comparisons of the proposed adsorbent and other adsorbent for the adsorption of  $Pb^{2+}$ ,  $Zn^{2+}$  and  $Cu^{2+}$ .

Adsorbent	Metal ions	$q_m$ (mg/g)	$K_L$ (L g <sup>-1</sup> )	Reference
Rice Husk	$Pb^{2+}$	0.651	186.67	[35]
	$Zn^{2+}$	19.74	0.066	
Aminated Polyacrylonitrile Nanofiber Mats	$Pb^{2+}$	15.75	22.90	[36]
Kaolinite	$Cu^{2+}$	30.40	23.70	[29]
	$Pb^{2+}$	7.75	0.003	
	$Zn^{2+}$	4.95	0.001	
ARS- $Fe_3O_4$	$Cu^{2+}$	4.42	0.001	This work
	$Pb^{2+}$	21.7	1.00	
	$Zn^{2+}$	50.0	1.33	
	$Cu^{2+}$	22.7	0.33	

### 3.7. Adsorption kinetic modeling

Several models are available to study the adsorption mechanism and describe the corresponding experimental data. The most commonly models used are the pseudo-first-order and pseudo-second-order reaction rate equations developed by Ho and McKay [37].

Pseudo-first-order equation:

$$\log(q_e - q_t) = \log q_e - k_1 t \quad (5)$$

Pseudo-second-order equation:

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e} \quad (6)$$

where  $k_1$  and  $k_2$  are the adsorption rate constants,  $q_t$  is adsorption capacity at time  $t$ ,  $q_e$  is adsorption capacity at equilibrium condition.

To describe the adsorption behavior and rate, the data obtained from adsorption kinetic experiments were evaluated using pseudo-first-order and pseudo-second-order reaction rate models. Experimental results of the three metal ions fitted to the selected adsorption model are shown in Table 4.

Table 4 gives a summary of the models and the corresponding constants along with the correlation coefficients for the linear regression plots of the three tested metal ions. Higher values of  $R^2$  were obtained for pseudo-second order than for pseudo-first order adsorption rate models indicating that the adsorption rates of  $Zn^{2+}$ ,  $Cu^{2+}$  and  $Pb^{2+}$  onto ARS- $Fe_3O_4$  nanoparticles can be more appropriately described using the pseudo-second-order rate [37].

**Table 4.** Adsorption kinetic constants for Cu<sup>2+</sup>, Zn<sup>2+</sup> and Pb<sup>2+</sup> onto ARS-Fe<sub>3</sub>O<sub>4</sub> nanoparticles.

Metal ion	Pseudo-first-order model			Pseudo-second-order model			Intra-particle diffusion		
	k <sub>1</sub> (min <sup>-1</sup> )	q <sub>e</sub> (mg g <sup>-1</sup> )	R <sup>2</sup>	k <sub>2</sub> (g mg <sup>-1</sup> min <sup>-1</sup> )	q <sub>e</sub> (mg g <sup>-1</sup> )	R <sup>2</sup>	k <sub>i</sub> (g mg <sup>-1</sup> min <sup>-1</sup> )	C (mg g <sup>-1</sup> )	R <sup>2</sup>
Cu <sup>2+</sup>	0.22	1.1	0.982	0.47	9.80	1.00	0.288	8.66	0.998
Zn <sup>2+</sup>	0.02	137	0.996	0.90	8.33	0.999	0.412	6.99	0.978
Pb <sup>2+</sup>	0.07	0.5	0.978	1.1	29.4	1.00	0.066	28.69	0.993

Intra-particle diffusion is a transport process involving movement of species from the bulk of the solution to the solid phase. The intra-particle kinetic model is expressed by:

$$Q_t = k_i t^{1/2} + C \quad (7)$$

Where k<sub>i</sub> is an intra-particle diffusion rate constant and Q<sub>t</sub> is amount of adsorbate adsorbed at time t. Initially, the external surface adsorption, which is faster, is completed and then, the intra-particle diffusion is attained. A plot of the amount of analyte adsorbed, q<sub>t</sub> (mg g<sup>-1</sup>) vs. the square root of the time, gives the rate constant (slope of the plot) and the intercept is proportional to the boundary layer thickness.

Intra-particle diffusion [38] is a transport process involving movement of species from the bulk of the solution to the solid phase surface. The mechanism for adsorption of a metal ions on nanoparticles is assumed as a three-step process in which bulk diffusion, i.e. migration of the metal ions from the bulk of the solution to the boundary layer nearby the surface of the nanoparticle, is not considered. The first step is diffusion of metal ions through the boundary layer toward the surface of the adsorbent. The second step is the metal ions transfer from the exterior surface of the adsorbent particle to the interior pores of the particle through a pore diffusion or intra-particle diffusion mechanism. Finally, the adsorption occurs onto an active site of adsorbent via an ion exchange and/or a complexation process [39-41]. According to intra-particle diffusion model, the plot of uptake should be linear if intraparticle diffusion is involved in an adsorption process. If this line passes through the origin then intra-particle diffusion is the rate-controlling step. When the plot does not pass through the origin, this is indicative of some degree of boundary layer control. This shows that the intra-particle diffusion is not the only rate limiting step, but also other kinetic models may control the rate of adsorption, all of which may be operating simultaneously [38]. According to the intra-particle diffusion model, the slope of the

linearized plot characterizes the rate parameter of the diffusion, whereas the intercept is proportional to the boundary layer thickness. In this study, the correlation coefficient (R<sup>2</sup>) value of the model indicates the possibility of intra-particle diffusion (Table 4) for the metal ions adsorbed onto magnetic nanoparticles.

### 3.8. Desorption and reusability studies

In this regard, the reusability of the nanoparticles was an important factor to be studied. Possible desorption of Zn<sup>2+</sup>, Cu<sup>2+</sup> and Pb<sup>2+</sup> were tested by EDTA (0.01, 0.1 mol L<sup>-1</sup>) and HCl (0.01, 0.1 mol L<sup>-1</sup>) solutions. The desorption ratio was calculated as the ratio of the amount of metal ions in the desorption medium to the amount of metal ions initially adsorbed on ARS-Fe<sub>3</sub>O<sub>4</sub> nanoparticles. The results showed that the desorption ratios were about 101%, 94% and 102% (in HCl at 0.1 mol L<sup>-1</sup>) for Zn<sup>2+</sup>, Cu<sup>2+</sup> and Pb<sup>2+</sup>, respectively. The study revealed that the adsorbed Zn<sup>2+</sup>, Cu<sup>2+</sup> and Pb<sup>2+</sup> could be completely desorbed in the presence of HCl. In this study more than 94-102% of metal ions could be desorbed and recovered by 2 mL of HCl (0.1 mol L<sup>-1</sup>) in 15 minutes, when 50 µg of metal ions was already adsorbed on 25.0 mg [ARS]-Fe<sub>3</sub>O<sub>4</sub> nanoparticles.

The reusability of the adsorbents in several successive separation processes was tested and the result showed that the [ARS]-Fe<sub>3</sub>O<sub>4</sub> nanoparticles can be reused for three times without significant reduction in its removal capacity. After being used for three times, the adsorption efficiencies were reduced to about 5.5, 10.4 and 15.3 %, respectively, for Zn<sup>2+</sup>, Cu<sup>2+</sup> and Pb<sup>2+</sup>. Considering the reproducibility of the results (RSD), these data indicated that the adsorbent was better not to be used more than 3 times.

## 4. CONCLUSIONS

The ARS-Fe<sub>3</sub>O<sub>4</sub> nanoparticles were quite efficient as magnetic nano-adsorbents for fast adsorption of metal ions from aqueous solutions. The time required to achieve the adsorption equilibrium was 15, 10 and 5 minutes for Zn<sup>2+</sup>, Cu<sup>2+</sup> and Pb<sup>2+</sup>,



respectively. The adsorption of the tested metal ions on the surface of ARS-Fe<sub>3</sub>O<sub>4</sub> nanoparticles was concluded due to its complexation with Alizarin red S. The experimental data fitted with Langmuir and Freundlich models indicated that the adsorptions of Zn<sup>2+</sup>, Cu<sup>2+</sup> and Pb<sup>2+</sup> on ARS-Fe<sub>3</sub>O<sub>4</sub> nanoparticles are better described by the Langmuir model. The changes of enthalpy ( $\Delta H$ ) were determined to be 67.45 and 83.60 and 7.09 kJ mol<sup>-1</sup> for Zn<sup>2+</sup>, Cu<sup>2+</sup> and Pb<sup>2+</sup> in the same order. Kinetic data were appropriately fitted to the pseudo-second order adsorption rates. The HCl (0.1 mol L<sup>-1</sup>) solution was suitable for desorption of Zn<sup>2+</sup>, Cu<sup>2+</sup> and Pb<sup>2+</sup>; the reusability of ARS-Fe<sub>3</sub>O<sub>4</sub> was found to be for three times. It would be better to study the adsorption of these three metal ions simultaneously, this suggestion will be considered as a future study.

Considering the objective of the work that could be deduced from the title of the paper, a comparative study between Fe<sub>3</sub>O<sub>4</sub> and ARS-Fe<sub>3</sub>O<sub>4</sub> has not been performed. However, the results could be used for being compared with other dyes that have been used for modification of Fe<sub>3</sub>O<sub>4</sub> nanoparticles [42].

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